### GE Healthcare Life Sciences

#### Data file 11-0011-65 AC

#### Affinity chromatography

# MabSelect SuRe\*

MabSelect SuRe (Superior Resistance) is a member of the MabSelect\* family of affinity chromatography media for the capture of monoclonal antibodies (MAbs) at process scale. MabSelect SuRe is composed of a rigid, high-flow agarose matrix and alkali-stabilized protein A-derived ligand. This ligand provides greater stability than conventional protein A-based media under the alkaline conditions used in cleaning-in-place (CIP) protocols. The enhanced alkali stability of MabSelect SuRe improves process economy; cleaning can be performed with cost-effective reagents such as sodium hydroxide, which improves process economy and product quality.

#### Key performance characteristics of MabSelect SuRe are:

- Novel, alkali-stabilized protein A ligand allows the use of 0.1–0.5 M sodium hydroxide for CIP
- Improves product quality and reduces overall costs
- Novel ligand design gives enhanced protease resistance resulting in lower ligand leakage
- Generic elution conditions for different monoclonal antibodies enables platform approach to purification
- High dynamic binding capacity (DBC) reduces process time and amount of medium used
- High-flow agarose matrix allows processing of large volumes of feed

#### High stability in alkaline conditions

The MabSelect SuRe ligand was developed by protein engineering of one of the IgG-binding domains of Protein A. Amino acids particularly sensitive to alkali were identified and substituted with more stable ones. The final construct



Fig 1. MabSelect SuRe is designed for purification of large volumes of monoclonal antibodies and is resistant to cleaning- and sanitization-in-place using alkali.

is a tetramer of the engineered domain with a C-terminal cysteine, which enables single-point attachment to the matrix.

The ligand is produced by validated fermentation and downstream processes and the entire production process is free of components of mammalian origin. The resulting highly purified ligand is immobilized to the agarose matrix through a chemically stable thio-ether linkage.

The toxicology of the MabSelect SuRe ligand has been investigated in a toxicity study and is reported in Application note 11-0011-64. Although a high dose of the ligand was administered, no toxic effects of the ligand were observed.

MabSelect SuRe is stable under alkali conditions and has been tested for up to 200 cycles of CIP using 0.1 M NaOH. The combination of low ligand leakage and high DBC together with the high-flow matrix makes MabSelect SuRe an excellent choice for purification of MAbs at process scale.



# Rigid, highly cross-linked matrix allows high flow rates

The MabSelect family of media for process-scale purification of monoclonal antibodies comprises MabSelect, MabSelect Xtra™, MabSelect SuRe, and MabSelect SuRe LX. MabSelect is designed for high-throughput purification of monoclonal antibodies from large volumes of feed. MabSelect Xtra demonstrates even higher DBC and is also optimized for Fc-fusion proteins. For more information on MabSelect and MabSelect Xtra, refer to Data files 18-1149-94 and 11-0011-57 respectively.

MabSelect SuRe has been developed from the same rigid, highly cross-linked agarose matrix used for MabSelect. The matrix of MabSelect SuRe allows the use of higher flow rates in process-scale purifications of Mabs compared with conventional cross-linked agarose of similar porosity. MabSelect SuRe LX has been further developed from MabSelect SuRe to give even higher binding capacity at longer residence time. For more information on MabSelect SuRe LX, refer to Data file 28-9870-62.

The characteristics of MabSelect SuRe are summarized in Table 1.

Table 1. Characteristics of MabSelect SuRe

LigandAlkali-stabilized protein A-derived (E. coli)Ligand coupling methodEpoxy activationMatrixRigid, highly cross-linked agaroseAverage particle size (d <sub>sov</sub> )185 μmDynamic binding capacity2Approx. 30-35 mg human IgG/mL medium at 2.4 min residence time
MatrixRigid, highly cross-linked agaroseAverage particle size (d_sov)185 μmDynamic binding capacity2Approx. 30-35 mg human IgG/mL
Average particle size (d <sub>sov</sub> ) <sup>1</sup> 85 µm Dynamic binding capacity <sup>2</sup> Approx. 30-35 mg human IgG/mL
Dynamic binding capacity <sup>2</sup> Approx. 30-35 mg human IgG/mL
Recommended mobile 100–500 cm/h phase velocity <sup>3</sup>
Chemical stability Stable in all aqueous buffers commonly used in protein A chromatography.
pH working range 3–12
Cleaning-in-place stability 0.1–0.5 M NaOH
Delivery conditions 20% ethanol

 $^1$   $\,\,$  d\_{\_{\rm SOV}} is the median particle size of the cumulative volume distribution.

<sup>2</sup> Determined at 10% breakthrough by frontal analysis at a mobile phase velocity of 250 cm/h in a column with a bed height of 10 cm.

<sup>3</sup> Determined in an AxiChrom 300 column, bed height 20 cm, operating pressure less than 2 bar.

# High dynamic binding capacity after numerous CIP cycles

Cleaning-in-place is an essential step in the production of pure MAbs in industrial applications. The main drawback with using sodium hydroxide for CIP of conventional protein A-based media is the sensitivity of native and recombinant Protein A (rProtein A) to alkaline conditions. MabSelect SuRe, however, retains dynamic binding capacity after repeated CIP cycles with 0.1–0.5 M NaOH.

Figure 2 shows DBC (10% breakthrough) of polyclonal human IgG (*h*IgG) as a function of exposure to alkaline conditions.

MabSelect, with its conventional rProtein A ligand, was used for comparison. Approximately 85%–90% of the initial dynamic binding capacity of MabSelect SuRe is retained after numerous CIP cycles with sodium hydroxide.

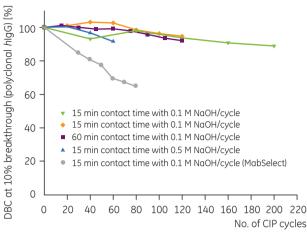


Fig 2. Dynamic binding capacity of MabSelect SuRe and MabSelect for polyclonal human IgG after CIP with 0.1–0.5 M NaOH for up to 200 cycles.

The dynamic binding capacity of MabSelect SuRe remains high after CIP in conjunction with purification of humanized  $IgG_1$  and  $IgG_4$  from clarified cell culture (Table 2). DBC was retained to approximately 85% of the initial binding capacity. The recovery of both MAbs was consistently over 95%.

Table 2. Effect of CIP cycles using 0.1 M NaOH on the DBC of MabSelect SuRe in the purification of  $\rm IgG_1$  and  $\rm IgG_4$ 

Antibody	CIP (no. of cycles × duration)	DBC (dynamic binding capacity [% of initial DBC])
IgG <sub>1</sub>	150 × 15 min	≥85%
IgG <sub>4</sub>	100 × 15 min	≥85%

## Increased residence time increases dynamic binding capacity

The already high dynamic binding capacity of MabSelect SuRe is further improved by increasing sample residence time on the medium. With a residence time of 2.4 min, the dynamic binding capacity at 10% breakthrough of humanized  $IgG_1$ , humanized  $IgG_4$ , and polyclonal hIgG is  $\geq 30 \text{ mg/mL}$  (Fig 3). Increasing the residence time to 4.8 min increases the dynamic binding capacity of the humanized immunoglobulins and hIgGto more than 38 mg/mL. At longer residence times or if even higher binding capacity is required, MabSelect SuRe LX is the recommended medium as it is optimized for long residence times.

#### Protease stability and low ligand leakage

The ligand construction of MabSelect SuRe has an increased stability towards proteases. All feeds contain proteases and with all protein ligands there is always a risk for proteolytic degradation. The degree of proteolytic activity can differ significantly between feedstocks. This is one of the most important contributions to ligand leakage from Protein A media.

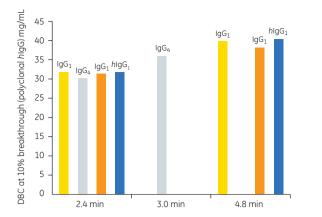
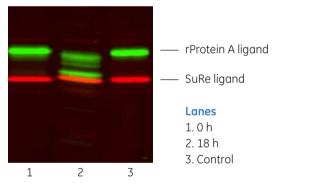


Fig 3. Dynamic binding capacity of MabSelect SuRe as a function of residence time of the protein on the medium.

Figure 4 shows the increased stability of MabSelect SuRe against proteases. Using fluroscent dyes, conventional rProtein A ligand (green) and SuRe ligand (red) were labelled. After incubation in CHO cell lysate,the conventional rProtein A ligand clearly showed degradation, whereas the SuRe ligand remained intact. The results illustrate why the use of MabSelect SuRe leads to lower ligand leaching levels. A normal range of leakage is estimated to be 5–20 ppm (ng ligand/mg IgG). However, leakage is affected by chromatographic running conditions and the composition of the feedstock.

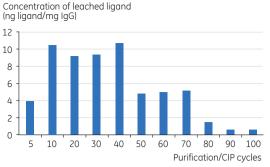


**Fig 4.** Electrophoresis of rProtein A ligand (marked with green fluorescent dye) and SuRe ligand (marked with red fluorescent dye). Ligands were incubated for 18 h at 37°C at pH 5 with or without 50% cell culture supernatant from non-MAb expressing CHO cells.

Figure 5 shows the ligand leakage from MabSelect SuRe over 100 cycles of purification of a monoclonal antibody from clarified cell culture. Fractions collected from the purification were analyzed by noncompetitive ELISA. Figure 5 confirms the low leakage of the MabSelect SuRe ligand over numerous purification/CIP cycles.

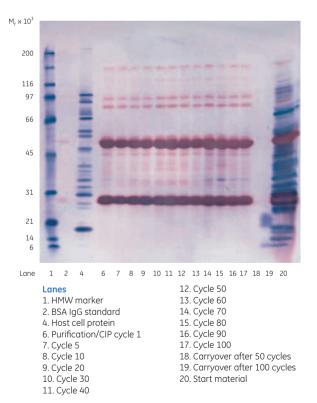
### Low risk of host cell protein contamination or carryover

Rigorous CIP or sanitization-in-place with sodium hydroxide reduces the risk of both contamination from host cell proteins and microbial growth in the packed column, as well as carryover in the product pools.



**Fig 5.** Ligand leakage (ppm) of MabSelect SuRe over 100 cycles of CIP in conjunction with the purification of humanized  $IgG_4$ . Cleaning-in-place was performed with 0.1 M NaOH and the contact time was 15 min/cycle.

Figure 6 is a Western blot of humanized  $IgG_4$  fractions eluted in the ligand-leakage study described above. The Western blot confirms that no contamination from host cell proteins or carryover is detected after 50–100 purification cycles on MabSelect SuRe (lanes 18 and 19). Comparison of the host cell protein standard in lane 4 with the purified  $IgG_4$  in lanes 6–17 obtained from 100 affinity purifications on MabSelect SuRe indicates no presence of the host cell proteins in the eluates. The absence of protein bands in lanes 18 (blank cycle after 50 cycles) and 19 (blank cycle after 100 cycles) indicates no carryover or cross-contamination between two consecutive purification cycles with an intermittent CIP cycle. Sample, data, and image were supplied by kind courtesy of Lonza Biologics plc, Slough, U.K.



**Fig 6.** Western blot of humanized  $IgG_4$  from 1–100 purification/CIP cycles on MabSelect SuRe. The Western blot was developed with two sets of polyclonal antibodies; one raised against the host cell proteins and another raised against the MAb. The presence of bovine serum albumin (BSA) and IgG in lane 2, as the negative and positive controls respectively, marks the specificity of the two sets of antibodies.

### Comparison of MabSelect SuRe with rProtein A-based media

Figures 7 and 8 show the performance of MabSelect SuRe and MabSelect in the purification of humanized  $IgG_1$  and  $IgG_4$  from HCCF (harvested cell culture fluid). Selectivity and specificity of the two media were comparable.

In a separate study, the purification of humanized IgG<sub>4</sub> expressed in cell culture fluid using MabSelect SuRe was compared to the purification performance of MabSelect and MabSelect Xtra. Purification performance of the three media was similar and contamination of host cell proteins was minimal as seen on the Western blot in Figure 9. Sample, data, and image were supplied by kind courtesy of Lonza Biologics plc, Slough, U.K.

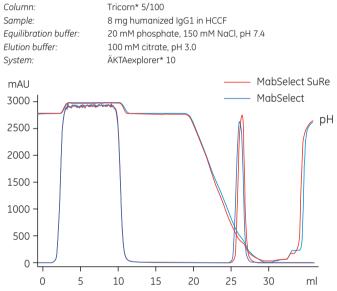


Fig 7. Similar desorption characteristics of MabSelect SuRe and MabSelect in the purification of humanized  $IgG_1$  from HCCF.

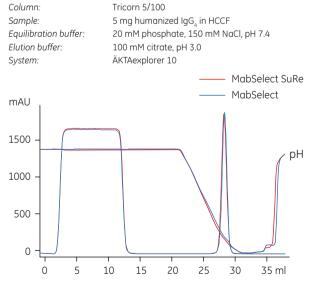
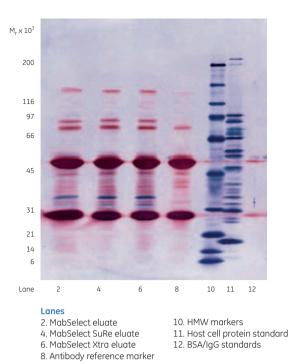


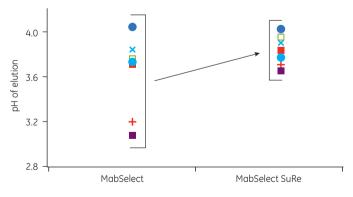
Fig 8. Similar desorption characteristics of MabSelect SuRe and MabSelect in the purification of humanized  ${\rm IgG}_{\rm a}$  from HCCF.



**Fig 9.** Western blot confirming the purity of humanized IgG<sub>4</sub> purified on MabSelect SuRe, MabSelect, and MabSelect Xtra.

#### **Generic elution conditions**

MabSelect SuRe has been shown to give generic elution conditions for different monoclonal antibodies, which is an advantage when designing generic purification platform processes. This feature is also correlated with the construction of the MabSelect SuRe ligand. In Figure 10, the elution pH for a range of different monoclonal antibodies is shown. With MabSelect (with a traditional rProtein A ligand) the different MAbs are eluted at different pH, but for MabSelect SuRe they are all eluted in a more narrow pH interval.



**Fig 10.** Scatter plot showing the distribution of elution, pH of various human antibodies, and Fc fusion proteins on MabSelect and MabSelect SuRe. Redrawn from (1), by courtesy of Amgen.

#### Operation Method development

MabSelect SuRe offers high selectivity, which renders efficiency related parameters such as sample load, flow rate, bead size and bed height less important for resolution.

The primary aim of method optimization is to establish the conditions that will bind the highest amount of target molecule, in the shortest time, and with the highest product recovery. The degree to which IgG binds to protein A varies with respect to both origin and antibody subclass. In general, however, all human or humanized antibodies, except for subclass 3, have a high affinity for protein A.

Typically, the clarified feedstock is loaded onto the column directly. After sufficient washing, the MAb is normally eluted at pH 3–4.

PreDictor\* 96-well filter plates or miniaturized columns, prefilled with MabSelect SuRe, are suitable for efficient highthroughput screening of chromatographic conditions during process development. Defined conditions can then be verified and optimized with HiTrap\* or HiScreen\* prepacked columns. An example of a high-throughput screening and optimization of MabSelect SuRe step is described in Application note 28-9468-58.

#### Cleaning and sanitization

Use of 0.1–0.5 M NaOH is recommended for cleaning and sanitization. Optimization of contact time, concentration, and frequency of CIP cycles is required to achieve the best possible results. For challenging feed-stocks, CIP protocols with reducing agent (e.g., thioglycerol or DTT) followed by 0.1-0.5 M NaOH is an option. A high throughput screening methodology, where numerous cleaning agents and sequences of cleaning steps can be evaluated in parallel using PreDictor 96-well filter plates, is described in Application Note 28-9845-64.

Effective sanitization of MabSelect SuRe is possible using a solution containing 0.1 M NaOH and 40% isopropyl alcohol.

#### Storage

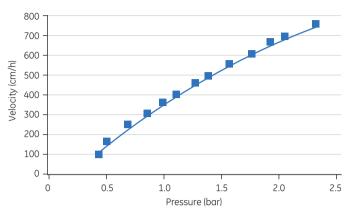
Recommended storage solutions for MabSelect SuRe are 20% ethanol or solutions containing 2% benzyl alcohol. The recommended storage temperature is 2°C to 8°C.

Recommendations for column packing, cleaning and sanitization, method design, and optimization can be found in the instructions delivered with each pack of medium.

#### Scale-up

After optimizing the antibody purification at laboratory scale, the process can be scaled up by keeping the residence time constant in order to maintain capacity. This can be achieved by increasing the column diameter, and keeping the mobile phase velocity and sample-to-bed volume ratio constant.

MabSelect SuRe is based on the same matrix as MabSelect and has similar pressure and flow characteristics. At process scale, the preferred packing technique is axial compression. Using AxiChrom\* columns with Intelligent Packing and preprogrammed packing methods for all MabSelect products, is the most optimal and fastest approach. For more details on packing in process-scale columns, see Application note 11-0007-52.



**Fig 11.** Pressure/flow profile for MabSelect SuRe in a packed bed (bed height 20 cm) in an AxiChrom 300 column (i.d. 300 mm).

#### Equipment

MabSelect SuRe can be used together with most equipment available for chromatography from laboratory scale to process scale. To ensure best performance at process scale, pack MabSelect SuRe to a bed height of 10–30 cm.

Recommended columns are listed in Table 3.

MabSelect SuRe is also available within the ReadyToProcess\* platform, with prepacked, prequalified and presanitized ReadyToProcess columns ranging in size from 1 to 20 L, designed for purification of biopharmaceuticals for clinical phase I and II studies.

 Table 3. Recommended columns for MabSelect SuRe. For maximum productivity

 and robust performance, bed heights of 10–30 cm are normally used

Column family range	Inner diameter (mm)
Lab scale:	
Tricorn	5, 10
HiScale*	16, 26, 50
Pilot and production scale:	
AxiChrom	50 - 1000
BPG*	100 – 300 <sup>†</sup>
Chromaflow*	400 – 800 <sup>‡</sup>

The pressure rating of BPG 450 is too low to use it with MabSelect SuRe media
 Larger pack stations might be required at larger diameters

#### Reference

1. Ghose, G., *et al.* Antibody variable region interactions with protein A: Implications for the development of generic purification processes. *Biotechnol. Bioeng.* **92**, 665-673 (2005).

### **Ordering Information**

Product	Pack size	Code No
MabSelect SuRe	25 mL	17-5438-01
	200 mL	17-5438-02
	1 L	17-5438-03
	5 L	17-5438-04
	10 L	17-5438-05
RTP MabSelect SuRe	1 L	28-9511-10
	2.5 L	28-9017-17
	10 L	28-9017-18
	20 L	28-9017-19
HiScreen MabSelect SuRe	1 × 4.7 mL	28-9269-77
HiTrap MabSelect SuRe	5 × 1 mL	11-0034-93
	5 × 5 mL	11-0034-95
PreDictor MabSelect SuRe	6 µL (4 × 96-well plates)	28-9258-23
	20 µL (4 × 96-well plates)	28-9258-24
	50 µL (4 × 96-well plates)	28-9258-25
PreDictor RoboColumn** MabSelect SuRe	50 µL (one row of 8 columns)	28-9862-03
	200 µl (one row of 8 columns)	28-9861-07

#### **Related literature**

Data files	
MabSelect SuRe LX	28-9870-62
MabSelect	18-1149-94
MabSelect Xtra	11-0011-57
AxiChrom columns	28-9290-41
BPG columns	18-1115-23
Chromaflow columns	18-1138-92
HiScale columns	28-9755-23
PreDictor 96-well filter plates and Assist software	28-9258-39
PreDictor RoboColumn	28-9886-34
HiTrap MabSelect, MabSelect Xtra, MabSelect SuRe	11-0034-90
HiScreen prepacked columns	28-9305-81
ReadyToProcess Columns	28-9159-87

### For local office contact information, visit **www.gelifesciences.com/contact**

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### imagination at work

MabSelect SuRe: studies on ligand toxicology, leakage, removal of leached ligand, and sanitization11-0011-64High-throughput screening of elution pH for monoclonal antibodies on MabSelect SuRe using PreDictor plates28-9277-92High-throughput screening and optimization of a protein A capture step in a monoclonal antibody process28-9468-58A flexible antibody purification process based on ReadyToProcess products28-9403-48Scale-up of a downstream monoclonal antibody purification process using HiScreen and AxiChrom columns28-9403-49Purification of a monoclonal antibody using ReadyToProcess columns28-9198-56High-throughput process development for design of cleaning-in-place protocols28-9403-58High-throughput process development with PreDictor plates, principles and methods28-9403-58	Application notes	
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Antibody purification, principles and methods 18-1037-46		28-9403-58
	Antibody purification, principles and methods	18-1037-46

All bulk media products are supplied in suspension in 20% ethanol. For additional information, please contact your local GE Healthcare representative.

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